INDUSTRIAL PROCESS

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SESSION 3 HEAT PROCESS

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Heat process

Flash smelting

Flash smelting (<u>Finnish</u>: *Liekkisulatus*) is a <u>smelting</u> process for <u>sulfur</u>-containing ores^[11] including <u>chalcopyrite</u>. The process was developed by <u>Outokumpu</u> in <u>Finland</u> and first applied at the <u>Harjavalta</u> plant in 1949 for smelting copper ore.^{[2][3]} It has also been adapted for <u>nickel</u> and <u>lead</u> production.^[2]

A second flash smelting system was developed by the International Nickel Company ('INCO') and has a different concentrate feed design compared to the Outokumpu flash furnace.^[4] The **Inco flash furnace** has end-wall concentrate injection burners and a central waste gas off-take,^[4] while the **Outokumpu flash furnace** has a water-cooled reaction shaft at one end of the vessel and a waste gas off-take at the other end.^[5] While the INCO flash furnace at Sudbury was the first commercial use of oxygen flash smelting,^[6] fewer smelters use the INCO flash furnace than the Outokumpu flash furnace.^[4]

Flash smelting with oxygen-enriched air (the 'reaction gas') makes use of the energy contained in the concentrate to supply most of the energy required by the furnaces.^{[4][5]} The concentrate must be dried before it is injected into the furnaces and, in the case of the Outokumpu process, some of the furnaces use an optional heater to warm the reaction gas typically to 100–450 °C.^[5]

The reactions in the flash smelting furnaces produce copper <u>matte</u>, iron oxides and <u>sulfur dioxide</u>. The reacted particles fall into a bath at the bottom of the furnace, where the iron oxides react with <u>fluxes</u>, such as <u>silica</u> and <u>limestone</u>, to form a <u>slag</u>.^[7]

In most cases, the slag can be discarded, perhaps after some cleaning, and the matte is further treated in converters to produce blister copper. In some cases where the flash furnaces are fed with concentrate containing a sufficiently high copper content, the concentrate is converted directly to blister in a single Outokumpu furnace^[8] and further converting is unnecessary.

The sulfur dioxide produced by flash smelting is typically captured in a <u>sulfuric</u> <u>acid plant</u>, removing the major environmental effect of smelting.^[9]

<u>Outotec</u>, formerly the technology division of Outokumpu, now holds Outokumpu's patents to the technology and licenses it worldwide. **Heat Treatment** is the controlled heating and cooling of metals to alter their physical and mechanical properties without changing the product shape. Heat treatment is sometimes done inadvertently due to manufacturing processes that either heat or cool the metal such as welding or forming.

Heat Treatment is often associated with increasing the strength of material, but it can also be used to alter certain manufacturability objectives such as improve machining, improve formability, restore ductility after a cold working operation. Thus it is a very enabling manufacturing process that can not only help other manufacturing process, but can also improve product performance by increasing strength or other desirable characteristics.

Steels are particularly suitable for heat treatment, since they respond well to heat treatment and the commercial use of steels exceeds that of any other material. Steels are heat treated for one of the following reasons:

- 1. Softening
- 2. Hardening
- 3. Material Modification

Common Heat Treatments

Softening: Softening is done to reduce strength or hardness, remove residual stresses, improve toughnesss, restore ductility, refine grain size or change the electromagnetic properties of the steel.

Restoring ductility or removing residual stresses is a necessary operation when a large amount of cold working is to be performed, such as in a cold-rolling operation or wiredrawing. <u>Annealing</u> — full Process, spheroidizing, normalizing and <u>tempering</u> — austempering, martempering are the principal ways by which steel is softened.

Hardening: Hardening of steels is done to increase the strength and wear properties. One of the pre-requisites for hardening is sufficient carbon and alloy content. If there is sufficient Carbon content then the steel can be <u>directly</u> <u>hardened</u>. Otherwise the surface of the part has to be Carbon enriched using some <u>diffusion treatment hardening</u> techniques.

Material Modification: Heat treatment is used to modify properties of materials in addition to hardening and softening. These processes modify the behavior of the steels in a beneficial manner to maximize service life, e.g., <u>stress relieving</u>, or strength properties, e.g., <u>cryogenic treatment</u>, or some other desirable properties, e.g., <u>spring aging</u>.

THERMODYNAMICS: HEAT

<u>←</u>

Processes with Heat and Work

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The Carnot Cycle

Though we have shown the net flow of energy and entropy, we haven't proposed a more specific mechanism for the heat engine. The most basic cycle is known as the Carnot cycle, and is simple if not completely accurate for a real engine. Still, it is beneficial to see a simplified picture to understand the basic concepts.

The Carnot cycle consists of four phases. Refer to as we trace the steps of the cycle. At point A, the gas (it needn't be a gas necessarily) is at temperature $\tau_{\rm h}$ with entropy $\sigma_{\rm L}$ where the latter represents the lowest entropy attained by the system during the cycle and is distinct from $\sigma_{\rm L}$. The gas is then expanded at constant temperature and the entropy is increased to $\sigma_{\rm H}$ at point B. The expansion is isothermal, that is, performed at a constant temperature.

Now, the gas is expanded further, but at constant entropy. The temperature falls to τ_{\perp} during this isentropic process and arrives at point C. The gas is then compressed isothermally to point D, and is compressed isentropically back to point A, thus completing one cycle.

The total work accomplished by the system can be written from our previous results as $W = \Delta \tau \times \sigma_h$. Looking at the figure again, we see that this is merely the area enclosed by the rectangle. This yields a nice graphical method of understanding a simple version of a heat engine.

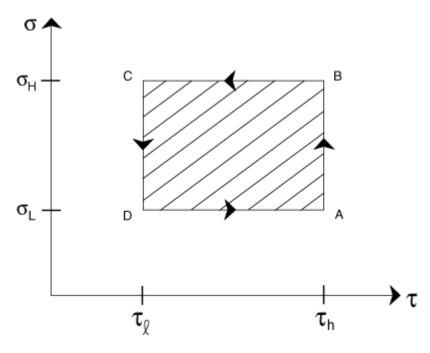


Figure %: A Carnot Cycle

Energies Revisited

We have stressed throughout that knowing well the energy identities makes problem solving much easier, and we have seen this in many of the problems we have tackled. It appears again here, as we discuss processes performed on a gas.

For an isothermal expansion or compression, we wish to deal with an energy where τ appears as a differential. Conventionally, the Helmholtz free energy is used. Barring any diffusive exchange, we can see that dF gives us dU - dQ, which is exactly the work done on the system.

For an isobaric process, we wish to use the Enthalpy, for the pressure appears in the differential there. This choice allows us to carefully account for the work done on the system and that done on the environment in a process.

For a process that is both isobaric and isothermal, it makes sense to look at the Gibbs Free Energy.

Therefore, while solving problems, look for what is being held constant so that you can make an appropriate choice of energy.

THERMODYNAMIC PROCESSES FOR AN IDEAL GAS

Process	<u>Isobaric</u>	<u>Isochoric</u>	<u>Isothermal</u>	Adiabatic
Variable =>	Pressure	Volume	Tempemature.	No Heat Flow
Quantity Constant =>	$\Box \mathbf{P} = 0$	□V = 0	□ T = 0	Q = 0
<u>n</u>	0	00	1	$\underline{\mathbf{y}} = \mathbf{C}_{\mathbf{p}}/\mathbf{C}_{\mathbf{v}}$
<u>First Law</u>	□U = Q - W	∪ U = Q W = 0	□ U = 0 Q = W	□ U = - W Q = 0
<u>Work</u> ₩=∫ <i>Pd</i> V	$P(V_2 - V_1)$	0	$P_1V_1\ln\!\left(\!\frac{V_2}{V_1}\right)$	$\frac{\boldsymbol{P}_1\boldsymbol{V}_1-\boldsymbol{P}_2\boldsymbol{V}_2}{\boldsymbol{\gamma}-\boldsymbol{1}}$
Heat Flow Q	$mC_p(T_2-T_1)$	$m C_{\nu} (T_2 - T_1)$	$P_1V_1\ln\!\left(rac{V_2}{V_1} ight)$	0
<u>Heat</u> <u>Capacity</u>	<i>C</i> _p	C _v	00	0
<u>Internal</u> <u>Energy</u>	$m C_v (T_2 - T_1)$	$m C_v (T_2 - T_1)$	0	$m C_{v} (T_2 - T_1)$
$\Delta U = U_2 - U_1$				
$\frac{\text{Enthalpy}}{\Delta H = H_2 - H_1}$ $H = U + PV$	$mC_p(T_2-T_1)$	$m C_p (T_2 - T_1)$	0	$m C_p (T_2 - T_1)$
<u>Entropy</u>		_		
	$mC_p \ln \frac{T_2}{T_1}$	$mC_v \ln \frac{T_2}{T_1}$	$nR\lnrac{V_2}{V_1}$	0*

PVⁿ = Constant

$\Delta S = S_2 - S_1$ $= \int dQ/T$				
Ideal Gas	$P_{1} = P_{2}$	$V_1 = V_2$	$T_1 = T_2$	$Q = 0$ $(S_1 = S_2) *$
<u>Relations</u>	$\frac{V_1}{T_1} = \frac{V_2}{T_2}$	$\frac{P_1}{T_1} = \frac{P_2}{T_2}$	$\boldsymbol{P}_1 \boldsymbol{V}_1 = \boldsymbol{P}_2 \boldsymbol{V}_2$ $\boldsymbol{P}_1 = \boldsymbol{V}_2$	$\boldsymbol{P}_1 \boldsymbol{V}_1^{\boldsymbol{\tau}} = \boldsymbol{P}_2 \boldsymbol{V}_2^{\boldsymbol{\tau}}$
$\frac{P_1V_1}{T_1} = \frac{P_2V_2}{T_2}$ $PV = N kT$	$\frac{T_1}{T_2} = \frac{V_1}{V_2}$	$\frac{\boldsymbol{T}_1}{\boldsymbol{T}_2} = \frac{\boldsymbol{P}_1}{\boldsymbol{P}_2}$	$\frac{P_1}{P_2} = \frac{V_2}{V_1}$	$\frac{T_1}{T_2} = \left(\frac{V_2}{V_1}\right)^{r-1}$

*	For	Adiabatic	Reversible	Processes
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 $\mathbf{n} \mathbf{c}_{\mathbf{p}} = \mathbf{m} \mathbf{C}_{\mathbf{p}}$ $\mathbf{n} \mathbf{c}_{\mathbf{v}} = \mathbf{m} \mathbf{C}_{\mathbf{v}}$ $\mathbf{c}_{\mathbf{p}} - \mathbf{c}_{\mathbf{v}} = \mathbf{R}$ $\mathbf{n} \mathbf{R} = \mathbf{N} \mathbf{k}$

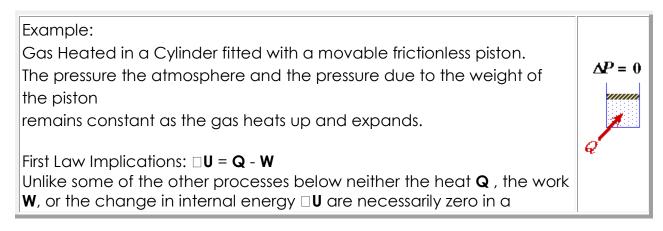
 $\Box = C_p/C_v = c_p/c_v = Ratio of Specific Heats$

 C_p = Constant Pressure Specific Heat Capacity (J/kg/ °C) C_v = Constant Volume Specific Heat Capacity (J/kg/ °C) c_p = Molar Constant Pressure Heat Capacity (J/mole/oC) c_v = Molar Constant Volume Heat Capacity (J/mole/oC)

Important Thermal Processes

<u>Isobaric</u>	<u>Isothermal</u>	<u>Isovolumetric</u>
Adiabatic	<u>Isoentropic</u>	<u>Polytropic</u>

ISOBARIC Pressure is Constant ($\Box P = 0$)



constant pressure process.

For an ideal gas, constant pressure <u>work</u> is easily determined, $W = \int P dV = P \Box V$

Part of the heat that flows into the system causes the temperature to rise, $\mathbf{Q} = \mathbf{n} \mathbf{c}_{\mathbf{p}} \Box \mathbf{T} = \mathbf{m} \mathbf{C}_{\mathbf{p}} \Box \mathbf{T}$, the rest goes into work.

ISOTHERMAL Temperature is Constant (\Box T = 0)

Example1: Boiling of water in the open air. In general most isobaric phase changes are isothermal. In this example the system does work as the steam-produced pushes against the atmosphere as it expands. Neither the heat Q , the work W , or the change in internal energy U are zero. In this case Q = mL _v since the water <u>changes phase</u> .	$\Delta T = 0$
Example 2: In general for an Ideal gas U is only a function of the temperature so that \Box U is always equal to zero for an isothermal process.Since \Box U = 0 then W = Q from the First Law. What has to happen for this process to be isothermal is that the gas in a cylinder is compressed slowly enough that heat flows out of the gas at the same rate at which is being done on the gas. The ideal gas law can be used to determine the <u>work</u> done W = PV ln(Vf/Vo) which is also the equation for Q . Note that P ₁ V ₁ = P ₂ V ₂ = nRT , the ideal gas law for an isothernal process.	wQ

See <u>Summery Table</u> for more change for an Ideal gas.

ISOCHORIC (Isovolumetric) Volume is constant $(\Box V = 0)$

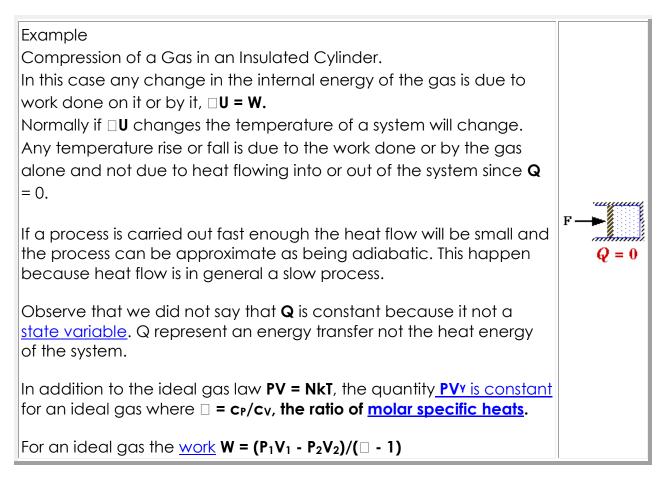
Example:

Heating of a Gas in a Rigid, Closed container.

In this case no work is done on the gas because $W = \int P dV = \int P 0 = 0$. As a result the FirstLaw implies that the change in internal energy must equal any heat flowing into or out of the system, $\Box U = Q = n c_v \Box T = m$ $C_v \Box T$.

Note that $V_1 = V_2 = nRT_1/P_1 = nRT_2/P_2$, the ideal gas law for constant volume process.

ADIABATIC No heat flows into or out of the system (Q = 0)



See <u>Summery Table</u> for more change for an Ideal gas.

 $\Delta V = 0$

ISOENTROPIC Entropy is constant (\Box S = 0)

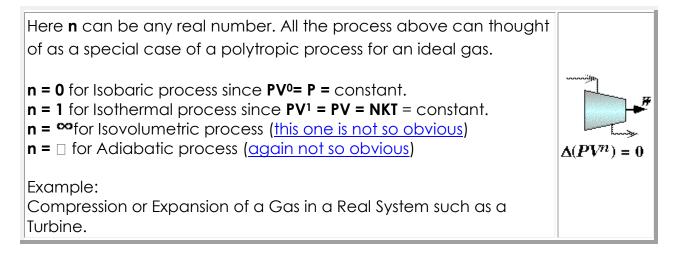
Example:

A Heat Engine in which the working fluid undergoes an Adiabatic <u>Reversible</u> cyclic process.

Any isoentropic process is also adiabatic since $\Box U = \int dQ/T$ and Q = 0. However, not all adiabatic process are isoentropic. Adiabatic free expansion is not isoentropic.

For a heat engine to be reversible, not only must the change in entropy of the working fluid be zero but also the net change of the entropy of the environment (heat reservoirs) must also be zero.

POLYTROPIC PVn is constant



Solids

Strong forces of attraction hold particles close together in fixed regular arrangement. The particles don't have much energy so only vibrate about their fixed positions.

ΔS :

Liquids

Weaker forces of attraction between particles than solids. particles are close together but can move past each other, and form irregular arrangements. They have more energy than the particles in a solid and move in random directions at low speeds

Gases

There are almost no forces of attraction between the particles. The particles have more energy than those in liquids and solids and are free to move and travel in random directions at high speeds

Boiling

Particles are give enough energy to overcome their attraction to each other and form big bubbles of gas (liquids)

Melting

Heat energy makes the particles vibrate faster until eventually the forces between them are overcome and the particles start to move around

Condensing/freezing

Bonds are forming between particles which releases energy

Specific Heat Capacity

The amount of energy needed to raise the temperature of 1kg of a substance by 1 degree

Specific Latent Heat

The amount of energy needed to change 1kg of a substance from one state to another without changing its temperature

Specific Latent Heat of Vaporisation

The amount of energy needed to change 1kg of material from liquid vapour to gas without changing its temperature (boiling)

Specific Latent Heat of Fusion

The amount of energy needed to change 1kg of material from a solid to a liquid without changing its temperature

Conduction

In solids

Convection

In liquids and gases

Dark, matt surfaces

good absorbers and good emitters

Light, shiny surfaces

Poor absorbers as they reflect lots. Poor emitters